# Gas chromatographic determination of vapour pressures of pheromone-like compounds II. ${ }^{\text {\# }}$ Alcohols 

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#### Abstract

The vapour pressures of $98(Z)$ - and $(E)$-monounsaturated $C_{10}-C_{18}$ alcohols were determined using a method based on gas chromatographic retention data. This method, by utilizing a non-polar HP-1 capillary column, five experimental temperatures, four reference compounds ( $C_{11}, C_{12}, C_{14}$ and $C_{16}$ alkanols) whose polarities approximated that of the test compounds and melting point corrections for compounds that are solids at ambient temperature, provided vapour pressures that agreed reasonably well with the available literature values. For alkenols belonging to structurally similar subseries, e.g., for $\omega-3$, $\omega-5$ and $\omega-7$ unsaturated derivatives, the vapour pressures may be represented over a range of pressure by simple equations in which the number of carbon atoms is a parameter.


## 1. Introduction

The saturation properties of pure liquids play a major role in both the understanding of fluid phase behaviour and the design and operation of a multitude of industrial processes [1,2]. Such properties are essential not only when used directly in calculations, but also when

[^0]used as input to variety of models and applications.

At present, there is an increasing need for vapour pressures of high-molecular-mass organic compounds at ambient temperatures $[3,4]$. One of the most important reasons for this is the increased public sensitivity to the effect of chemicals on health and the environment generally. As the vapour pressure of an organic chemical exerts a large influence on its dispersal in the environment, a knowledge of the vapour pressures should allow one not only to model the fate of organic pollutants $[5,6]$ but
also to optimize the use of ecologically friendly behaviour-modifying chemicals [7]. An impetus for developing more effective design for practical applications of these compounds is the continuing value of pheromones for monitoring insect flight activity and the recent commercial success in controlling several pests by permeating the air with their sex pheromones [7]. Both the release rates and, in the case of blends, the release ratios of pheromone components from dispensers are governed, for the most part, by the vapour pressures of the compounds. It appears that environmental concerns are weighing against the use of traditional pesticides and expectations are [8] that pheromones will capture about $15-40 \%$ of the insecticide market within 10 years. Thus, an understanding of the pheromone evaporative process can aid in the optimization of selectivity conditions and the minimization of the loss of the biological activity of synthetic pheromone blends.

The vapour pressures of compounds of low volatility are commonly determined by either gas saturation $[9,10]$ or effusion [11] methods. Gas chromatography (GC) is an alternative method for measuring vapour pressures [12,13], offering advantages in terms of speed, solute sample size, purity and stability requirements. It is based on the use of a non-polar stationary phase and isothermal conditions such that a compound's GC retention time is related directly to its vapour pressure. The GC method has been used to study polychlorinated biphenyls and dioxins $[14,15]$, herbicide esters [12], organophosphorus pesticides [16], tetraorganostannanes [17], linear alkylbenzenes [18] and fatty acid methyl esters [19]. Using this approach, we have obtained [20] some vapour pressure data on pheromone-like acetates.

In this paper we show that the GC method yields equally good results in determining equilibrium vapour pressures of more polar compounds, viz. monounsaturated $\left(\mathrm{C}_{10}-\mathrm{C}_{18}\right)$ pheromone-like alcohols. The extensive set of 98 compounds studied also allowed the influence of subtle structural differences in chain length and the positions of double bonds on vapour pressures to be revealed.

## 2. Experimental

### 2.1. Chromatography

Samples were analysed on a Hewlett-Packard HP 5890 chromatograph equipped with a $3 \mathrm{~m} \times$ 0.31 mm I.D. fused-silica capillary column (cross-linked $5 \%$ methylsilicone, HP-1, film thickness $0.52 \mu \mathrm{~m}$ ) with split injection and a flame ionization detector. The length of the column employed ( 3 m ) is a compromise between the need for acceptable resolution when working with mixtures and the need to avoid prohibitively long retention times, particularly at lower temperatures. The chromatograph was operated isothermally with a hydrogen flow-rate of $5 \mathrm{ml} / \mathrm{min}$ at $10^{\circ} \mathrm{C}$ intervals in the range $50-$ $160^{\circ} \mathrm{C}$ as specified. $\mathrm{C}_{11}, \mathrm{C}_{12}, \mathrm{C}_{14}$ and $\mathrm{C}_{16}$ alkanols were used as reference standards. Retention times were determined on a HewlettPackard HP 5895A ChemStation. Adjusted retention times were calculated by subtracting the retention time of methane from the retention time of the chemical. As recommended [13], long retention times of compounds producing unsymmetrical peaks at low temperatures were not taken at the peak maximum, but were estimated at the centre of gravity of the peak. The reproducibility of retention time measurements expressed as the relative standard deviation of at least three measurements for each compound was $0.03 \%$.

### 2.2. Chemicals

The alcohols were either obtained from the Research Institute for Plant Protection (IPODLO) (Wageningen, Netherlands) and used as received or synthesized in our laboratory. In the latter instance, the purity of the chemicals was at least $97 \%$ as determined by capillary GC. Condensed nomenclature for alcohols is used: the letters after the colon indicate the functional type ( $\mathrm{OH}=$ alcohol), the number between the dash and colon indicate the number of carbon atoms in the chain and the letters and numbers before the dash indicate the configuration and
position of the double bonds, e.g., Z3-10:OH is ( $Z$ )-3-decenol.

### 2.3. Data treatment

The method has been discussed in detail by Bidleman [13] and Hinckley et al. [21] and will therefore be only briefly reviewed here. At a constant temperature, the vapour pressures of a test and of a reference compound (subscripts $T$ and $R$, respectively) are related by the ratio of their latent heats of vaporization:
$\ln P_{\mathrm{T}}=\frac{\Delta H_{\mathrm{T}}}{\Delta H_{\mathrm{R}}} \cdot \ln P_{\mathrm{R}}+C$
where $\Delta H$ is the latent heat of vaporization and $C$ is a constant. A similar equation has been developed for the GC (adjusted) retention times $t^{\prime}$ :
$\ln \left(\frac{t_{\mathrm{T}}^{\prime}}{t_{\mathrm{R}}^{\prime}}\right)=\left(1-\frac{\Delta H_{\mathrm{T}}}{\Delta H_{\mathrm{R}}}\right) \ln P_{\mathrm{R}}-C$
Hence, a plot of $\ln \left(t_{\mathrm{T}}^{\prime} / t_{\mathrm{R}}^{\prime}\right)$ versus $\ln P_{\mathrm{R}}$ should have a slope $1-\Delta H_{\mathrm{T}} / \Delta H_{\mathrm{R}}$ and an intercept $-C$. Eq. 1 can then be used to determine the vapour pressure of the test compound at any temperature if the vapour pressure of the reference compound at that temperature is known.

Since the GC method gives the subcooled liquid vapour pressure (defined as the liquid vapour pressure extrapolated below the melting point) [22], it was necessary to convert the literature-based solid vapour pressures ( $P_{\mathrm{S}}$ ) into subcooled liquid vapour pressures ( $P_{\mathrm{L}}$ ) by using the equation developed by Mackay et al. [23]:
$\ln \left(\frac{P_{\mathrm{S}}}{P_{\mathrm{L}}}\right)=-\frac{\Delta S_{\mathrm{F}}}{R}\left(\frac{T_{\mathrm{M}}}{T}-1\right)$
where $T_{\mathrm{M}}$ and $T$ are the absolute melting and ambient temperatures, respectively, $R$ is the gas constant and $\Delta S_{\mathrm{F}}$ is the entropy of fusion. The usually employed "average" value of $\Delta S_{\mathrm{F}}=56.5$ $\mathrm{J} / \mathrm{K} \cdot \mathrm{mol}$ (or the corresponding value $\Delta S_{\mathrm{F}} / R=$ 6.79) seems to be too low for alcohols, however. Based on the value of enthalpy of fusion ( $\Delta H_{\mathrm{F}}$ ) published [24] for 1-hexadecanol ( $34.286 \mathrm{~kJ} /$ mol ), $\Delta S_{\mathrm{F}}$ for this compound amounts 106.34
$\mathrm{J} / \mathrm{K} \cdot \mathrm{mol}$ and, as a consequence, $\Delta S_{\mathrm{F}} / R=$ 12.789. Hence this constant was used to convert literature $P_{\mathrm{S}}$ values of 1-hexadecanol and 1pentadecanol into $P_{\mathrm{L}}$.

### 2.4. Statistical analysis

The data were subjected to statistical analyses utilizing the Statgraphics Plus 7.0 software package (Manugistic, Rockville, MD, USA).

## 3. Results and discussion

The accuracy of the GC method as represented by Eqs. 1 and 2 depends to a large extent on two factors: (i) the accuracy of the $P_{\mathrm{R}}$ values and (ii) the similarity of infinity dilution activity coefficients $\gamma$ in the stationary phase between the test and reference compounds to which Eq. 2 is applied. Strictly, an additional term, $-\ln \left(\gamma_{\mathrm{T}} /\right.$ $\gamma_{\mathrm{R}}$ ), should appear (see discussion in Ref. [21]) on the right-hand side of this equation and only when $\gamma_{\mathrm{T}} \sim \gamma_{\mathrm{R}}$ (or at least $\gamma_{\mathrm{T}} / \gamma_{\mathrm{R}} \sim$ constant) can the use of Eq. 1 lead to reasonable results. As values of $\gamma$ on a squalane liquid phase have been found [25] to range from 0.48 to 0.73 for hydrocarbons and from 17 to 34 for alcohols, the frequently employed reference hydrocarbons seemed to be disqualified for our purposes. Therefore, we chose to use $n$-alkanols (i.e., compounds of the same chemical class as the test compounds) as the reference standards. When literature vapour pressure values were being selected for the reference $n$-alkanols, some judgment was necessary. We favoured recent static measurements [26] that have been especially focused on the low vapour pressure field. The literature values of the four reference compounds given in Table 1 in the form of the Antoine equation are thus from a single report. In most instances vapour pressures were calculated from the Antoine constants by interpolation. In those instances where some extrapolation was necessary ( $14: \mathrm{OH}, 15: \mathrm{OH}$ and $16: \mathrm{OH}$ ), the temperature range of extrapolation was usually less than 40 K .

As the choice of the $P_{\mathrm{R}}$ is critical for the

Table 1
Vapour pressures ( $P_{\mathrm{R}}$ ) of the reference $n$-alkanols

| Alkanol | Constants of the Antoine <br> equation |  | $P_{\mathrm{R}}\left(25^{\circ} \mathrm{C}\right)$ <br> $(\mathrm{Pa})$ |  |
| :--- | :--- | :--- | :--- | :--- |
|  | $A$ | $B$ | $C$ |  |
| $11: \mathrm{OH}$ | 7.094 | 2105.005 | 176.145 | 0.4255 |
| 12:OH | 6.860 | 2011.634 | 162.769 | 0.1402 |
| 14:OH | 6.916 | 2217.995 | 165.381 | 0.01844 |
| 16:OH | 5.964 | 1781.618 | 120.726 | $0.00207^{\mathrm{b}}$ |

${ }^{\mathrm{a}}$ Ref. [26]; $\log P(\mathrm{kPa})=A-B /(t+C)$.
${ }^{\mathrm{b}}$ Vapour pressure is for the subcooled liquid; it was calculated from the original solid vapour pressure $\left(5.4726 \cdot 10^{-4}\right.$ Pa ) using Eq. 3 and m.p. $56^{\circ} \mathrm{C}$.
accuracy of vapour pressures determined by the comparative GC method, the literature $P_{\mathrm{R}}$ data were checked for internal consistency. Examination of the logarithm of vapour pressure (corrected for melting point) as a function of the number of carbon atoms in alkanol series (Fig. 1) confirms that an excellent linear correlation, $\ln P=(-1.0675 \pm 0.0058) n_{\mathrm{C}}+(10.8973 \pm$ $0.0734)\left(n=7\right.$, S.E. $\left.=0.0374, r^{2}=0.9999\right)$, does exist.


Fig. 1. Liquid vapour pressures ( Pa ) $\left(25^{\circ} \mathrm{C}\right)$ of alkanols [25] as a function of the number of carbon atoms. $\square=$ Original (solid) vapour pressures of $15: \mathrm{OH}$ and $16: \mathrm{OH}$.

Table 2
Adjusted GC retention times ( min ) of the $n$-alkanols

| Alkanol | $80^{\circ} \mathrm{C}$ | $90^{\circ} \mathrm{C}$ | $100^{\circ} \mathrm{C}$ | $110^{\circ} \mathrm{C}$ | $120^{\circ} \mathrm{C}$ |
| :--- | ---: | ---: | ---: | ---: | ---: |
| $9: \mathrm{OH}$ | 0.773 | 0.482 | 0.332 | 0.237 | 0.172 |
| $10: \mathrm{OH}$ | 1.553 | 0.926 | 0.605 | 0.409 | 0.283 |
| $11: \mathrm{OH}$ | 3.162 | 1.800 | 1.123 | 0.724 | 0.481 |
| $12: \mathrm{OH}$ | 6.557 | 3.541 | 2.122 | 1.313 | 0.837 |
| $14: \mathrm{OH}$ | 26.696 | 13.305 | 7.385 | 4.242 | 2.256 |
| $15: \mathrm{OH}$ | 53.448 | 25.600 | 13.698 | 7.600 | 4.379 |
| $16: \mathrm{OH}$ | 110.337 | 50.162 | 25.846 | 13.914 | 7.757 |

### 3.1. Validation of the method

Six $n$-alkanols with known $P_{\mathrm{L}}$ [26] were chromatographed along with the 14:OH reference, and $P_{\mathrm{GC}}$ values at $25^{\circ} \mathrm{C}$ were calculated from the relative retention data (Table 2) using Eqs. 1 and 2. In Fig. 2, these $P_{\mathrm{GC}}$ values are compared with $P_{\mathrm{L}}$. As can be scen, the regression line obtained closely parallels the $y=x$ line. The equation of the regression line by a linear leastsquares fit is

$$
\begin{gather*}
\ln \left[P_{\mathrm{L}}(\mathrm{~Pa})\right]=(1.02536 \pm 0.0049) \ln P_{\mathrm{GC}}  \tag{4}\\
\left(n=6, \text { S.E. }=0.0402, r^{2}=0.9999\right)
\end{gather*}
$$



Fig. 2. Logarithmic plot of the literature vapour pressures $P_{\mathrm{L}}$ of alkanols ( $25^{\circ} \mathrm{C}$ ) vs. the corresponding $P_{\mathrm{GC}}$ data (Eq. 1) from the present work. The regression line (solid) and $y=x$ line (dashed) are shown.
with a slope nearly equal to 1 . Note that in Eq. 4 the intercept has not been included at the $0.05 \%$ probability level. The quality of fit produced by the proposed vapour pressure correlation is excellent, thus demonstrating the validity of the GC method even for polar compounds.

Another noteworthy feature of this correlation is that it appears to be applicable over a range of pressures that covers three orders of magnitude. Table 3 presents a comparison between the GCbased and literature vapour pressure data. Our corrected (Eq. 4) vapour pressures differ from those given by N'Guimbi et al. [26] by values ranging from $0.6 \%$ (for $10: \mathrm{OH}$ ) to $5.3 \%$ (for 12:OH). In addition to the original database [26] employed in deriving Eq. 4, Table 3 also includes a complete data set [3] obtained from the Chebyshev-type polynomial in $x$ of degree 3 by extrapolation. This polynomial has been proposed to allow extrapolation for about 150 K with fair confidence. The slightly lower (about $10 \%$ ) but consistently similar vapour pressure values following from the use of this equation might be regarded as a notable agreement between the two literature data sets. It is noticable that vapour pressures of $10: \mathrm{OH}(1.233 \mathrm{~Pa})$ and $12: \mathrm{OH}(0.1328 \mathrm{~Pa})$ following from the use of Eq. 4 compare favourably with the values 1.190 and 0.1397 Pa obtained [27] for these compounds from a simultaneous correlation of vapour pres-
sure and thermal data. Hence it appears that the GC method is capable of yielding vapour pressures of saturated alcohols with an error below $10 \%$.

This conclusion finds further support in the estimated heats of vaporization. In deriving vapour pressures from GC retention time data, $\Delta H_{\mathrm{T}} / \Delta H_{\mathrm{R}}$, the ratio of the enthalpies of vaporization of a test to that of the reference compound is obtained. Hence, by utilizing the literature [28] experimental $\Delta H_{\mathrm{R}}$ value for our reference standard, $14: \mathrm{OH}\left(102.2 \pm 2.4 \mathrm{~kJ} \mathrm{~mol}^{-1}\right)$, the remaining enthalpies of vaporization of alkanols may be calculated from the $\Delta H_{\mathrm{T}} / \Delta H_{\mathrm{R}}$ ratios given in Table 3. The results calculated by this approach are $72.17 \mathrm{~kJ} \mathrm{~mol}^{-1}$ for $9: O H$, $79.27 \mathrm{~kJ} \mathrm{~mol}^{-1}$ for $10: \mathrm{OH}$ and $91.69 \mathrm{~kJ} \mathrm{~mol}^{-1}$ for $12: \mathrm{OH}$. These values compare well with the corresponding calorimetric data, viz. $76.86 \pm$ $0.75,81.50 \pm 0.75$ and $91.96 \pm 0.59 \mathrm{~kJ} \mathrm{~mol}^{-1}$, respectively, yielding a maximum error of $6.1 \%$.

### 3.2. Vapour pressures of alkenols

Vapour pressures of all measured alkenols were determined by the same approach as described above for saturated compounds. Taking advantage of the internal consistency of the vapour pressure data for saturated derivatives demonstrated above, the test compounds were

Table 3
Parameters of Eq. 2 and vapour pressures $\left(25^{\circ} \mathrm{C}\right)$ of the $n$-alkanols

| Alkanol ${ }^{\text {a }}$ | $\Delta H_{\mathrm{T}} / \Delta H_{\mathrm{R}}$ | C | $P \cdot 1000(\mathrm{~Pa})$ |  |  |  | Error ${ }^{\text {e }}$ <br> (\%) |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  |  | Eq. 1 | Eq. 4 | Exp. ${ }^{\text {b }}$ | Exp. ${ }^{\text {d }}$ |  |
| 9:OH | 0.7062 | 4.1446 | 3760 | 3888 | 3738 | 3334 | 4.0 |
| 10:OH | 0.7756 | 3.3008 | 1226 | 1233 | 1241 | 1087 | -0.6 |
| 11:OH | 0.8379 | 2.4614 | 412.9 | 403.7 | 425.0 | 378.1 | -5.0 |
| 12:OH | 0.8972 | 1.6137 | 139.6 | 132.8 | 140.2 | 136.1 | -5.3 |
| 15:OH | 1.0493 | -0.7941 | 6.846 | 6.033 | $5.894^{\text {c }}$ | 5.335 | 2.4 |
| 16:OH | 1.1007 | -1.6180 | 2.446 | 2.100 | $2.069^{\text {c }}$ | 1.842 | 1.5 |

${ }^{2}$ Standard 14:OH.
${ }^{\mathrm{b}}$ Ref. [25].
${ }^{\text {c }}$ Corrected by using Eq. 3
${ }^{\mathrm{d}}$ Ref. [3].
${ }^{c}$ Error $=100\left(P_{\mathrm{GC}}-P_{\mathrm{EXP}}\right) / P_{\mathrm{EXP}} ; P_{\mathrm{EXP}}$ taken from Ref. [25].

Table 4
GC data and vapour pressures $\left(25^{\circ} \mathrm{C}\right)$ of decenols

| Alcohol | Relative retention time ${ }^{\text {a }}$ |  |  |  |  | $P(\mathrm{~Pa})$ |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | $50^{\circ} \mathrm{C}$ | $60^{\circ} \mathrm{C}$ | $70^{\circ} \mathrm{C}$ | $80^{\circ} \mathrm{C}$ | $90^{\circ} \mathrm{C}$ | Eq. 1 | Eq. 4 |
| 23-10:OH | 0.128 | 0.146 | 0.168 | 0.189 | 0.210 | 1.669 | 1.691 |
| E3-10:OH | 0.125 | 0.142 | 0.163 | 0.183 | 0.204 | 1.704 | 1.727 |
| Z4-10:OH | 0.135 | 0.153 | 0.174 | 0.193 | 0.214 | 1.536 | 1.553 |
| E4-10:OH | 0.141 | 0.160 | 0.179 | 0.198 | 0.218 | 1.432 | 1.445 |
| Z5-10:OH | 0.144 | 0.162 | 0.183 | 0.202 | 0.223 | 1.406 | 1.418 |
| E5-10:OH | 0.147 | 0.165 | 0.185 | 0.205 | 0.225 | 1.367 | 1.378 |
| Z6-10:OH | 0.147 | 0.166 | 0.186 | 0.206 | 0.227 | 1.380 | 1.391 |
| E6-10:OH | 0.147 | 0.165 | 0.185 | 0.205 | 0.225 | 1.365 | 1.376 |
| 27-10:OH | 0.153 | 0.171 | 0.192 | 0.212 | 0.232 | 1.311 | 1.320 |
| E7-10:OH | 0.153 | 0.171 | 0.191 | 0.210 | 0.229 | 1.294 | 1.303 |
| 28-10:OH | 0.175 | 0.195 | 0.217 | 0.237 | 0.258 | 1.109 | 1.112 |
| E8-10:OH | 0.165 | 0.183 | 0.204 | 0.224 | 0.244 | 1.187 | 1.192 |

${ }^{\text {a }}$ Standard $12: \mathrm{OH}$.
chromatographed using four reference standards: 11:OH (for $\mathrm{C}_{12}$ alkenols), 12: OH (for $\mathrm{C}_{10}, \mathrm{C}_{13}$ and $\mathrm{C}_{14}$ alkenols), 14:OH (for $\mathrm{C}_{15}$ and $\mathrm{C}_{16}$ alkenols) and 16:OH (for $\mathrm{C}_{18}$ alkenols).

The relative retention times and calculated
vapour pressures for $\mathrm{C}_{10}, \mathrm{C}_{12}, \mathrm{C}_{13}, \mathrm{C}_{14}, \mathrm{C}_{15}, \mathrm{C}_{16}$ and $\mathrm{C}_{18}$ alkenols are listed in Tables 4-10. Inspection of these tables reveals that the vapour pressures of all alkenols are similar to those of the corresponding alkanols. In spite of this, two

Table 5
GC data and vapour pressures $\left(25^{\circ} \mathrm{C}\right)$ of dodecenols

| Alcohol | Relative retention time ${ }^{\text {a }}$ |  |  |  |  | $P(\mathrm{~Pa})$ |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | $60^{\circ} \mathrm{C}$ | $70^{\circ} \mathrm{C}$ | $80^{\circ} \mathrm{C}$ | $90^{\circ} \mathrm{C}$ | $100^{\circ} \mathrm{C}$ | Eq. 1 | Eq. 4 |
| Z2-12:OH | 2.034 | 1.961 | 1.894 | 1.827 | 1.780 | 0.167 | 0.160 |
| Z2-12:OH | 2.083 | 2.002 | 1.933 | 1.854 | 1.806 | 0.162 | 0.155 |
| Z3-12:OH | 1.768 | 1.726 | 1.691 | 1.649 | 1.624 | 0.204 | 1.196 |
| E3-12:OH | 1.719 | 1.682 | 1.646 | 1.606 | 1.591 | 0.212 | 0.204 |
| Z4-12:OH | 1.793 | 1.743 | 1.701 | 1.652 | 1.612 | 0.196 | 0.188 |
| E4-12:OH | 1.896 | 1.832 | 1.775 | 1.715 | 1.665 | 0.181 | 0.173 |
| Z5-12:OH | 1.864 | 1.803 | 1.753 | 1.698 | 1.662 | 1.187 | 0.179 |
| E5-12:OH | 1.944 | 1.870 | 1.811 | 1.745 | 1.701 | 0.175 | 0.167 |
| Z6-12:OH | 1.867 | 1.800 | 1.753 | 1.697 | 1.664 | 0.187 | 0.179 |
| E6-12:OH | 1.913 | 1.839 | 1.787 | 1.726 | 1.673 | 0.178 | 0.170 |
| Z7-12:OH | 1.901 | 1.829 | 1.780 | 1.720 | 1.672 | 0.181 | 0.173 |
| E7-12:OH | 1.951 | 1.871 | 1.813 | 1.748 | 1.700 | 0.174 | 0.166 |
| Z8-12:OH | 2.002 | 1.922 | 1.855 | 1.789 | 1.738 | 1.169 | 0.162 |
| E8-12:OH | 2.002 | 1.914 | 1.855 | 1.784 | 1.732 | 0.169 | 0.162 |
| Z9-12:OH | 2.078 | 1.986 | 1.920 | 1.840 | 1.789 | 0.161 | 0.154 |
| E9-12:OH | 2.096 | 1.998 | 1.924 | 1.837 | 1.775 | 0.156 | 0.149 |
| Z10-12:OH | 2.402 | 2.273 | 2.171 | 2.065 | 1.979 | 0.132 | 0.125 |
| E10-12:OH | 2.246 | 2.128 | 2.041 | 1.946 | 1.886 | 1.145 | 0.138 |

[^1]Table 6
GC data and vapour pressures $\left(25^{\circ} \mathrm{C}\right)$ of tridecenols

| Alcohol | Relative retention time ${ }^{\text {a }}$ |  |  |  |  | $P(\mathrm{~Pa})$ |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | $70^{\circ} \mathrm{C}$ | $80^{\circ} \mathrm{C}$ | $90^{\circ} \mathrm{C}$ | $100^{\circ} \mathrm{C}$ | $110^{\circ} \mathrm{C}$ | Eq. 1 | Eq. 4 |
| Z7-13:OH | 1.762 | 1.721 | 1.675 | 1.633 | 1.590 | 0.0673 | 0.0628 |
| E7-13:OH | 1.817 | 1.769 | 1.713 | 1.666 | 1.619 | 0.0639 | 0.0596 |
| Z9-13:OH | 1.890 | 1.839 | 1.776 | 1.719 | 1.674 | 0.0607 | 0.0565 |
| E9-13:OH | 1.939 | 1.856 | 1.790 | 1.728 | 1.678 | 0.0575 | 0.0534 |
| Z11-13:OH | 2.266 | 2.177 | 2.077 | 1.999 | 1.920 | 0.0472 | 0.0436 |
| E11-13:OH | 2.167 | 2.077 | 1.982 | 1.900 | 1.833 | 0.0491 | 0.0455 |

${ }^{2}$ Standard 12:OH.
subtle trends are apparent in all series considering the influence of double bond position: (i) the vapour pressures of series members with a double bond located near the centre of the carbon chain are generally higher than those of the corresponding saturated compounds and (ii) the
vapour pressures of isomers with a double bond positioned on the second carbon atom of the chain (irrespective of the end of the molecule from which the numbering starts) are either close to or lower than those of the saturated compounds. It appears that the double bond position

Table 7
GC data and vapour pressures $\left(25^{\circ} \mathrm{C}\right)$ of tetradecenols

| Alcohol | Relative retention time ${ }^{\text {a }}$ |  |  |  |  | $P(\mathrm{~Pa})$ |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | $80^{\circ} \mathrm{C}$ | $90^{\circ} \mathrm{C}$ | $100^{\circ} \mathrm{C}$ | $110^{\circ} \mathrm{C}$ | $120^{\circ} \mathrm{C}$ | Eq. 1 | Eq. 4 |
| Z2-14:OH | 3.820 | 3.538 | 3.299 | 3.113 | 2.911 | 0.0211 | 0.0191 |
| E2-14:OH | 3.883 | 3.586 | 3.345 | 3.140 | 2.925 | 0.0203 | 0.0184 |
| Z3-14:OH | 3.389 | 3.186 | 3.013 | 2.847 | 2.685 | 0.0256 | 0.0234 |
| E3-14:OH | 3.286 | 3.083 | 2.912 | 2.767 | 2.609 | 0.0267 | 0.0243 |
| Z4-14:OH | 3.358 | 3.157 | 2.966 | 2.811 | 2.650 | 0.0256 | 0.0233 |
| E4-14:OH | 3.526 | 3.289 | 3.079 | 2.902 | 2.723 | 0.0234 | 0.0213 |
| Z5-14:OH | 3.408 | 3.217 | 3.017 | 2.843 | 2.663 | 0.0246 | 0.0224 |
| E5-14:OH | 3.551 | 3.308 | 3.096 | 2.917 | 2.729 | 0.0230 | 0.0209 |
| Z6-14:OH | 3.343 | 3.138 | 2.954 | 2.798 | 2.634 | 0.0257 | 0.0234 |
| E6-14:OH | 3.462 | 3.243 | 3.050 | 2.865 | 2.686 | 0.0240 | 0.0218 |
| Z7-14:OH | 3.340 | 3.134 | 2.959 | 2.798 | 2.634 | 0.0258 | 0.0235 |
| E7-14:OH | 3.485 | 3.259 | 3.057 | 2.883 | 2.704 | 0.0239 | 0.0217 |
| Z8-14:OH | 3.412 | 3.209 | 3.004 | 2.840 | 2.665 | 0.0246 | 0.0224 |
| E8-14:OH | 3.616 | 3.301 | 3.087 | 2.922 | 2.719 | 0.0220 | 0.0200 |
| Z9-14:OH | 3.512 | 3.285 | 3.079 | 2.898 | 2.725 | 0.0236 | 0.0215 |
| E9-14:OH | 3.622 | 3.376 | 3.157 | 2.961 | 2.768 | 0.0222 | 0.0202 |
| Z10-14:OH | 3.682 | 3.473 | 3.223 | 3.016 | 2.819 | 0.0217 | 0.0196 |
| E10-14:OH | 3.731 | 3.464 | 3.221 | 3.025 | 2.815 | 0.0211 | 0.0191 |
| Z11-14:OH | 3.881 | 3.587 | 3.335 | 3.117 | 2.909 | 0.0200 | 0.0181 |
| E11-14:OH | 3.834 | 3.548 | 3.300 | 3.079 | 2.864 | 0.0201 | 0.0182 |
| Z12-14:OH | 4.346 | 4.024 | 3.714 | 3.447 | 3.185 | 0.0169 | 0.0153 |
| E12-14:OH | 4.102 | 3.774 | 3.495 | 3.250 | 3.004 | 0.0180 | 0.0163 |

[^2]Table 8
GC data and vapour pressures $\left(25^{\circ} \mathrm{C}\right)$ of pentadecenols

| Alcohol | Relative retention time $^{\mathrm{a}}$ |  |  |  |  | $P(\mathrm{~Pa})$ |  |  |
| :--- | :--- | :--- | :--- | :--- | :--- | :--- | :--- | :--- |
|  | $90^{\circ} \mathrm{C}$ | $100^{\circ} \mathrm{C}$ | $110^{\circ} \mathrm{C}$ | $120^{\circ} \mathrm{C}$ | $130^{\circ} \mathrm{C}$ |  | Eq. 1 | Eq. 4 |
| Z9-15:OH | 1.633 | 1.598 | 1.564 | 1.533 | 1.505 |  | 0.00917 | 0.00814 |
| E9-15:OH | 1.692 | 1.649 | 1.605 | 1.568 | 1.536 | 0.00851 | 0.00754 |  |
| Z10-15:OH | 1.696 | 1.651 | 1.608 | 1.574 | 1.541 | 0.00845 | 0.00749 |  |
| E10-15:OH | 1.729 | 1.681 | 1.638 | 1.593 | 1.557 | 0.00815 | 0.00721 |  |
| Z11-15:OH | 1.768 | 1.721 | 1.676 | 1.629 | 1.590 | 0.00794 | 0.00702 |  |
| E11-15:OH | 1.769 | 1.721 | 1.673 | 1.623 | 1.581 | 0.00781 | 0.00691 |  |
| Z12-15:OH | 1.841 | 1.790 | 1.735 | 1.677 | 1.639 | 0.00739 | 0.00652 |  |
| E12-15:OH | 1.830 | 1.771 | 1.714 | 1.660 | 1.614 | 0.00730 | 0.00644 |  |
| Z13-15:OH | 2.071 | 1.988 | 1.915 | 1.849 | 1.792 | 0.00617 | 0.00542 |  |
| E13-15:OH | 1.955 | 1.880 | 1.811 | 1.744 | 1.69 | 0.00654 | 0.00576 |  |

${ }^{3}$ Standard 14:OH.

Table 9
GC data and vapour pressures $\left(25^{\circ} \mathrm{C}\right)$ of hexadecenols

| Alcohol | Relative retention time ${ }^{\text {a }}$ |  |  |  |  | $P(\mathrm{~Pa})$ <br> Eq. 1 |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | $100^{\circ} \mathrm{C}$ | $110^{\circ} \mathrm{C}$ | $120^{\circ} \mathrm{C}$ | $130^{\circ} \mathrm{C}$ | $140^{\circ} \mathrm{C}$ |  | Eq. 4 |
| Z3-16:OH | 2.973 | 2.801 | 2.673 | 2.524 | 2.401 | 0.00329 | 0.00285 |
| E3-16:OH | 2.900 | 2.741 | 2.605 | 2.465 | 2.343 | 0.00336 | 0.00291 |
| Z4-16:OH | 2.919 | 2.758 | 2.629 | 2.486 | 2.364 | 0.00337 | 0.00292 |
| E4-16:OH | 3.054 | 2.872 | 2.719 | 2.559 | 2.422 | 0.00302 | 0.00261 |
| Z5-16:OH | 2.944 | 2.779 | 2.639 | 2.494 | 2.369 | 0.00327 | 0.00283 |
| E5-16:OH | 3.033 | 2.851 | 2.703 | 2.546 | 2.412 | 0.00307 | 0.00265 |
| Z6-16:OH | 2.854 | 2.704 | 2.575 | 2.440 | 2.320 | 0.00348 | 0.00301 |
| E6-16:OH | 2.962 | 2.794 | 2.657 | 2.506 | 2.378 | 0.00323 | 0.00279 |
| Z7-16:OH | 2.809 | 2.664 | 2.545 | 2.414 | 2.299 | 0.00362 | 0.00314 |
| E7-16:OH | 2.993 | 2.798 | 2.659 | 2.507 | 2.377 | 0.00312 | 0.00270 |
| Z8-16:OH | 2.849 | 2.702 | 2.576 | 2.433 | 2.323 | 0.00350 | 0.00303 |
| E8-16:OH | 2.967 | 2.799 | 2.656 | 2.510 | 2.377 | 0.00321 | 0.00278 |
| Z9-16:OH | 2.880 | 2.711 | 2.586 | 2.447 | 2.335 | 0.00344 | 0.00298 |
| E9-16:OH | 3.001 | 2.825 | 2.679 | 2.521 | 2.393 | 0.00312 | 0.00270 |
| Z10-16:OH | 2.962 | 2.795 | 2.658 | 2.506 | 2.377 | 0.00323 | 0.00279 |
| E10-16:OH | 3.058 | 2.873 | 2.719 | 2.563 | 2.426 | 0.00302 | 0.00261 |
| Z11-16:OH | 3.050 | 2.870 | 2.719 | 2.572 | 2.430 | 0.00308 | 0.00266 |
| E11-16:OH | 3.125 | 2.930 | 2.757 | 2.604 | 2.457 | 0.00288 | 0.00248 |
| Z12-16:OH | 3.191 | 2.997 | 2.822 | 2.665 | 2.510 | 0.00282 | 0.00243 |
| E12-16:OH | 3.198 | 2.996 | 2.810 | 2.651 | 2.499 | 0.00276 | 0.00238 |
| Z13-16:OH | 3.330 | 3.110 | 2.922 | 2.746 | 2.588 | 0.00261 | 0.00224 |
| E13-16:OH | 3.294 | 3.066 | 2.884 | 2.705 | 2.544 | 0.00260 | 0.00224 |

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Table 10
GC data and vapour pressures $\left(25^{\circ} \mathrm{C}\right)$ of octadecenols

| Alcohol | Relative retention time ${ }^{\text {a }}$ |  |  |  |  | $P(\mathrm{~Pa})$ |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | $120^{\circ} \mathrm{C}$ | $130^{\circ} \mathrm{C}$ | $140^{\circ} \mathrm{C}$ | $150^{\circ} \mathrm{C}$ | $160^{\circ} \mathrm{C}$ | Eq. 1 | Eq. 4 |
| Z3-18:OH | 2.676 | 2.500 | 2.400 | 2.288 | 2.200 | 0.000377 | 0.000309 |
| E3-18:OH | 2.583 | 2.448 | 2.346 | 2.244 | 2.149 | 0.000406 | 0.000333 |
| Z9-18:OH | 2.465 | 2.339 | 2.254 | 2.160 | 2.083 | 0.000453 | 0.000373 |
| E9-18:OH | 2.596 | 2.455 | 2.366 | 2.247 | 2.157 | 0.000402 | 0.000330 |
| Z11-18:OH | 2.534 | 2.405 | 2.311 | 2.216 | 2.130 | 0.000431 | 0.000354 |
| E11-18:OH | 2.637 | 2.497 | 2.391 | 2.275 | 2.181 | 0.000386 | 0.000316 |
| Z13-18:OH | 2.712 | 2.555 | 2.439 | 2.326 | 2.221 | 0.000363 | 0.000296 |
| E13-18:OH | 2.753 | 2.585 | 2.463 | 2.342 | 2.234 | 0.000345 | 0.000282 |

${ }^{\mathrm{a}}$ Standard $16: \mathrm{OH}$.
relative to both the polar and non-polar ends of the molecule is significant. As illustrated in Figs. 3 and 4, these trends may be observed both for the $Z$ - and $E$-isomers in all the series investigated.

For homologous subseries such as $Z$ - or $E$ isomers of $7-10: \mathrm{OH}, 9-12: \mathrm{OH}, 11-14: \mathrm{OH}$ and 13-16: OH ( $\omega-3$ unsaturation), $\quad 5-10: \mathrm{OH}, \quad 7-$ $12: \mathrm{OH}, 9-14: \mathrm{OH}$ and $11-16: \mathrm{OH}$ ( $\omega-5$ unsatura-


Fig. 3. Vapour pressures (Eq. 4) for ( $Z$ )-alkenols plotted against the respective double bond position. $\square=$ Decenols; $\bullet=$ dodecenols; $\boldsymbol{\Delta}=$ tetradecenols; $\diamond=$ pentadecenols; $\square=$ hexadecenols. Dashed lines show the vapour pressures of the corresponding saturated compounds.
tion) and $3-10: \mathrm{OH}, 5-12: \mathrm{OH}, 9-14: \mathrm{OH}$ and $11-$ $16: \mathrm{OH}$ ( $\omega-7$ unsaturation), the double bond is at a constant position with respect to the non-polar end of the molecule. Analysis of the double bond effect in these subseries reveals that the vapour pressures of alkenols having different positions of unsaturation decrease in the order $\omega-7>\omega-5>\omega-3>$ saturated. The empirical relationships given by the $\ln P$ vs. $n_{\mathrm{C}}$ expression


Fig. 4. Vapour pressures (Eq. 4) for ( $E$ )-alkenols plotted against the respective double bond position. $\quad=$ Decenols; $\bullet=$ dodecenols; $\boldsymbol{\Delta}=$ tetradecenols; $\diamond=$ pentadecenols; $\square=$ hexadecenols. Dashed lines show the vapour pressures of the corresponding saturated compounds.

Table 11
Proposed relationships for predicting vapour pressures at $25^{\circ} \mathrm{C}$

| Alcohol <br> subseries | $\operatorname{Ln}[P(P a)]=a-b n_{\mathrm{c}}$ | S.E. | $r^{2}$ |  |
| :--- | :--- | :--- | :--- | :--- |
|  | $a$ | $b$ |  |  |
| Saturated | $10.772 \pm 0.135$ | $1.058 \pm 0.010$ | 0.0458 | 0.9998 |
| $\omega-3-(Z)$ | $10.904 \pm 0.065$ | $1.064 \pm 0.005$ | 0.0220 | 1.0000 |
| $\omega-3-(E)$ | $10.844 \pm 0.081$ | $1.060 \pm 0.006$ | 0.0276 | 0.9999 |
| $\omega-5-(Z)$ | $10.805 \pm 0.018$ | $1.046 \pm 0.001$ | 0.0061 | 1.0000 |
| $\omega-5-(E)$ | $10.849 \pm 0.020$ | $1.053 \pm 0.002$ | 0.0067 | 1.0000 |
| $\omega-7-(Z)$ | $10.995 \pm 0.222$ | $1.053 \pm 0.017$ | 0.0751 | 0.9995 |
| $\omega-7-(F)$ | $11.178 \pm 0.307$ | $1.071 \pm 0.023$ | 0.1040 | 0.9991 |

${ }^{\text {a }}$ Number of data points, $n=6$.
${ }^{b}$ S.E. $=$ standard error of estimate.
were obtained from analyses of the calculated (Tables 4-10) $\ln P$ data. The relevant equations, listed in Table 11, may be used to estimate vapour pressures for any set of $\omega-3, \omega-5$ and $\omega-7$ alkenols. The quality of the fit obtained with MAD (mean average deviation) $2.3 \%$ ( $\omega-3$ ), $1.9 \%(\omega-5)$ and $4.8 \%$ ( $\omega-7$ ) combined with the convenience of only one substance-specific input variable makes this an attractive approach in predicting vapour pressures of some other structurally similar derivatives.

At this point some comment should be made regarding literature vapour pressure values of unsaturated alcohols. To our knowledge, only four of the alkenols investigated in this work had literature data available for comparison. Heath and Tumlinson [29] determined the vapour pressures of Z7-12:OH, Z9-14:OH, Z11-14:OH and $\mathrm{Z} 11-16: \mathrm{OH}$ as $1.25,0.177,0.160$ and 0.039 Pa , respectively. They carried out these determinations on capillary liquid crystal GC columns at "room temperature", which probably corresponded to $30^{\circ} \mathrm{C}$. At that temperature our GC method yields vapour pressures of $0.344,0.044$, 0.037 and 0.0057 Pa , respectively, for the same compounds. Hence our values are significantly (3.6-6.8 times) lower than those in Ref. [29]. Note, however, that a high degree of correlation exists between both data sets. The linear fit
may be expressed as $\ln P=(1.1716 \pm 0.0666)$
$\ln P_{\text {Heath }}-(1.231 \pm 0.137)(n=4$, S.E. $=0.164$, $r^{2}=0.9936$ ).

By utilizing the reliable literature [26] values at $30^{\circ} \mathrm{C}$ (see Table 1) for $12: \mathrm{OH}(0.266 \mathrm{~Pa})$ and $14: \mathrm{OH}\left(0.0366 \mathrm{~Pa}\right.$ ), the ratio $P_{\text {alkenol }} / P_{\text {alkanol }}$ for compounds with the same number of carbon atoms may be adopted as an approximate measure of the "effect of non-terminal monounsaturation". This vapour pressure ratio following from our data is about $1.2-1.3$, which seems to be a reasonable value considering its similarity to the corresponding values common for non-terminal alkene [1] and unsaturated acetate series [20]. On the other hand, the ratio of 4.7-4.8 which follows from the use of the data from Ref. [29] appears to be unrealistically high. The reasons for this discrepancy are not clear. However, besides the imprecisely defined temperature they used, another factor might be important, viz. the use of cholesteryl $p$-chlorocinnamate as a stationary phase. It may be that the polar alcohols interact in a specific manner with this phase and then this factor would account for the differences in the two studies.

As the errors in the reported vapour pressures depend both on experimental uncertainties and on the accuracy of the literature vapour pressure data adopted for the reference standards, it is difficult to determine any inherent error in the present method for alcohols. Some discussion is possible, however: as to the latter error factor, recent inter-laboratory data [25,27] for $10: \mathrm{OH}$ and $12: \mathrm{OH}$ agree to within $\pm 5 \%$, which may be regarded as a very good agreement. Hence the differences between our data and those taken from the literature for alkanols are generally not greater than the experimental errors (see Table 3 ). On the other hand, when admitting a propagation of errors, the uncertainty might reach about $10 \%$. Moreover, the vapour pressures for $15: \mathrm{OH}$ and $16: \mathrm{OH}$ were obtained by (prudent) extrapolation and additionally corrected for melting points. It is unlikely that they are in serious error (see the internal homogeneity of the alkanol data illustrated in Fig. 1), but we have to accept their lower accuracy. Taken
together, we assume that, at worst, the crrors may combine to give an overall uncertainty in vapour pressures of about $15 \%$.

## 4. Conclusions

This study has demonstrated the successful application of the capillary GC method to the determination of the vapour pressures of unsaturated alcohols whose generally low thermal stability causes difficulties in direct measurements by conventional physico-chemical methods. The method yields reasonable vapour pressure values for both the alkanols and alkenols at $25^{\circ} \mathrm{C}$ provided that a compound of similar structure and polarity is used as the reference standard. It is hoped that these new values may considerably extend the database for the vapour pressures of alcohols, and enable entomologically oriented chemists to study and model the physical behaviour of pheromone-like compounds in the environment more accurately.
The method is currently being used to determine vapour pressures of unsaturated aldehydes and will be the subject of a separate report.

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## References

[1] R.C. Reid, J.M. Prausnitz and B.E. Poling, The Properties of Gases and Liquids, McGraw-Hill, New York, 4th ed., 1987.
[2] R.D. Shaver, R.L. Robinson, Jr., and K.A.M. Gasem, Fluid Phase Equilib., 64 (1991) 141.
[3] D. Ambrose, J.H. Ellender and C.H.S. Sprake, J. Chem. Thermodyn., 6 (1974) 909.
[4] R.D. Gray, Jr., J.L. Heidman, R.D. Springer and C. Tsonopoulos, Fluid Phase Equlib., 53 (1989) 355.
[5] D. Mackay and S. Paterson, Environ. Sci. Technol., 25 (1991) 427.
[6] D. Mackay, S. Paterson and W.Y. Shiu, Chemosphere, 24 (1992) 695.
[7] J.H. Tumlinson, in R.L. Ridgway, R.M. Silverstein and M.N. Iscoe (Editors), Behavior-Modifying Chemicals for Insect Management -Applications of Pheromones and Other Attractants, Marcel Dekker, New York, 1990, Ch. 5.
[8] A. Shani, Role of Pheromones in Integrated Pest Management, Institutes for Applied Research, Ben-Gurion University of the Negev, Beer-Sheva, Israel, 1991.
[9] W.F. Spencer and M.M. Cliath, Residue Rev., 85 (1983) 57.
[10] W.J. Sonnefeld, W.H. Yoller and W.E. May, Anal. Chem., 55 (1983) 275.
[11] J.J. Murray, R.F. Pottie and C. Pupp, Can. J. Chem., 52 (1974) 557.
[12] D.J. Hamilton, J. Chromatogr., 195 (1980) 75.
[13] T.F. Bidleman, Anal. Chem., 56 (1984) 2490.
[14] J.W. Westcott and T.F. Bidleman, J. Chromatogr., 210 (1981) 331.
[15] B.D. Eitzer and R.A. Hites, Environ. Sci. Technol., 22 (1988) 1362.
[16] Y.-H. Kim, J.E. Woodrow and J.N. Seiber, J. Chromatogr., 314 (1984) 37.
[17] D. Hawker, Chemosphere, 25 (1992) 427.
[18] P.M. Sherblom, P.M. Gschwend and R.P. Eganhouse, J. Chem. Eng. Data, 37 (1992) 394.
[19] S. Husain, P.N. Sarma, G.Y.S.K. Swamy and K. Sita Devi, J. Am. Oil Chem. Soc., 70 (1993) 149.
[20] B. Koutek, M. Hoskovec, K. Konečný and J. Vrkoč, J. Chromatogr., 626 (1992) 215.
[21] D.A. Hinckley, T.F. Bidleman, W.T. Foreman and J.R. Tushall, J. Chem. Eng. Data, 35 (1990) 232.
[22] W.Y. Shin and D. Mackay, J. Phys. Chem. Ref. Data, 15 (1986) 911.
[23] D. Mackay, A. Bobra, D.W. Chan and W.Y. Shin, Environ. Sci. Technol., 16 (1982) 645.
[24] D.R. Lide (Editor), CRC Handbook of Chemistry and Physics, CRC Press, Boca Raton, FL, 72nd cd., 199192.
[25] T. Nitta, K. Morinaga and T. Katayama, Ind. Eng. Chem. Fundam., 21 (1982) 296.
[26] J. N'Guimbi, H. Kaseghari, I. Mokbel and J. Jose, Thermochim. Acta, 196 (1992) 367.
[27] K. Růžička and V. Majer, Fluid Phase Equilib., 28 (1986) 253.
[28] M. Mansson, P. Sellers, G. Stridh and S. Sunner, J. Chem. Thermodyn., 9 (1977) 91.
[29] R.R. Heath and J.H. Tumlinson, J. Chem. Ecol., 12 (1986) 2081.


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    ${ }^{*}$ For Part I, see Ref. [20].

[^1]:    ${ }^{a}$ Standard 11:OH.

[^2]:    ${ }^{2}$ Standard $12: \mathrm{OH}$.

[^3]:    ${ }^{2}$ Standard $14: O H$.

